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# The Apparent Molal Volumes of Aqueous Solutions of NaCl, KCl, MgCl<sub>2</sub>, Na<sub>2</sub>SO<sub>4</sub>, and MgSO<sub>4</sub> from 0 to 1000 Bars at 0, 25, and 50 $^{\circ}C^{\dagger}$

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The densities of aqueous solutions of NaCl, KCl, MgCl<sub>2</sub>, Na<sub>2</sub>SO<sub>4</sub>, and MgSO<sub>4</sub> have been measured with a high pressure magnetic float densimeter from 0 to 1000 bars, 0.01 to 1.0 *m* ionic strength, and at 0, 25, and 50  $^{\circ}$ C. The relative apparent molal volumes,  $\phi_V(P) - \phi_V(0)$ , of these solutions have been fitted to an equation of the form  $\phi_{\rm V}(P)$  $-\phi_{v}(0) = \phi_{v}^{0}(P) - \phi_{v}^{0}(0) + Sm^{1/2}$  where the relative infinite dilution partial molal volumes,  $\phi_V^0(P) - \phi_V^0(0)$ , and the slopes S are functions of applied pressure and temperature. The pressure, temperature, and concentration dependence of the apparent molal volumes are briefly discussed.

Although there are reliable density and apparent molal volume data for many electrolytes at 1 atm (9, 11), little reliable data are available at high pressures. In our recent studies of the volume properties of multicomponent electrolyte solutions (13, 15) we have been examining the use of Young's rule (18) in predicting the properties of seawater. In order to predict the apparent molal volumes of seawater at elevated pressures (3), we had a need for reliable volume data on sea salts (NaCl, KCl, MgCl<sub>2</sub>, Na<sub>2</sub>SO<sub>4</sub>, and MgSO<sub>4</sub>). The present paper contains results on the apparent molal volumes of these salts from 0 to 1000 bars applied pressure, 0.01 to 1.0 ionic strength (to 2.0 ionic strength for NaCl), and 0, 25, and 50 °C.

### **Experimental Section**

The high pressure magnetic float densimeter used in this study is described in detail elsewhere (12). The high pressure densimeter consists essentially of a 1 atm densimeter (8) enclosed in a nonmagnetic bomb with optical ports to observe the motion of the float. The apparatus consists of a pressure bomb, a magnetic float, and auxiliary measuring and control systems.

The pressure bomb used in this study was machined from beryllium copper. The cylindrical bomb contains two plugs seated with O rings to form a vessel of 170 cm<sup>3</sup>. The magnetic float is made of thick-wall (0.4 cm) Pyrex glass and contains an Alnico-5 bar magnet. The volume of the float is 58.7672 cm<sup>3</sup> at 0 °C and 1 atm.

The pressure bomb was completely immersed in a 30-L constant temperature bath controlled to  $\pm 0.001 \,^{\circ}\text{C}$  with a Hallikainen Thermotrol. The temperature of the bath was set to ±0.005 °C with a platinum resistance thermometer (calibrated by the National Bureau of Standards, 1968 temperature scale). A 2800-bar Enerpac hand pump was used to generate pressure. A 1400-bar Heise Bourdon tube gauge was used to set the pressure. The Heise gauge was calibrated with a Harwood Engineering deadweight tester. The pressures were found to be reproducible to  $\pm 0.5$  bars from 0 to 1000 bars and are thought to be accurate to 1.4 bars.

lon-exchanged (18 M $\Omega$ ) water (Millipore-Super Q system) was used in the calibration runs and in the preparation of the solutions. Reagent grade salts were used, without further purification, for preparation of the solutions. The solutions of NaCl, KCl,  $Na_2SO_4$ , and  $MgSO_4$  were analyzed by evaporation to dryness. The MgCl<sub>2</sub> solutions were analyzed gravimetrically with AgNO<sub>3</sub>,

The calibration of the densimeter (2, 3) was made with ionexchanged water using the densities of water from the soundderived equation of state (4). The calibration results (2) indicate that the precision of the densities is  $\pm 3$  ppm at a given temperature and  $\pm 8$  ppm over the entire temperature range. The accuracy of the densities is thought to be  $\sim$ 30 ppm at 1000 bars applied pressure. An error of  $\pm 30$  ppm in density is equivalent to an error of  $\pm 0.3$  cm<sup>3</sup> mol<sup>-1</sup> at 0.1 m and  $\pm 0.03$  cm<sup>3</sup> mol<sup>-1</sup> at 1.0 *m* in  $\phi_V$  for 1–1 electrolytes.

<sup>†</sup> Taken in part from the dissertation submitted by Robert T. Emmet in partial fulfillment of the requirements for the degree of Doctor of Philosophy, University of Miami

Table I. The Apparent Molal Volumes of Aqueous Salt Solutions as a Function of Concentration and Pressure at 0 °C

				A. (NaCI)				
<i>P</i> , bar	<i>m</i> = 0.03027	<i>m</i> = 0.1299	<i>m</i> = 0.2507	$\phi_{V}(NaCl)$ m = 0.3852	<i>m</i> = 0.7766	<i>m</i> = 0.9630	<i>m</i> = 1.307	<i>m</i> = 2.008
0.00.4	12 200	12 607	12 052	14 279	15.090	15 436	16.040	17 189
0.00	14.009	14 071	15.552	14,279	15.005	16.040	10.040	17.102
100.90	14.550	14.07 1	15.149	14.033	15.790	16 622	17 101	19 150
199.80	15.700	15.000	15.010	15.324	10.007	10.032	17.121	10.109
300.20	16.697	15.929	16.450	15.768	16.827			
401.00	17.281	16.375	16.954	16.009	17.335	17.713	18.096	19.044
501.10		16.738	17.464	—	17.880	18.202	18.531	
601.00	17.530	17.203	17.996	—	18.230	18.664	19.935	19.829
701.60	18.176	17.635	18.438		18.647	19.101	19.353	20.185
802.00	18.246	17.970	18,935	_	19.032	19.510	19.728	20.528
901 70	18 579	18 244	19 250	_	19 420	19.877	20.066	20.840
1001.20	18.878	_	19.655		19.757	_	20.406	21.136
				$\phi_{V}(KCI)$				
<i>P</i> , bar	<i>m</i> = 0.1	1655 m =	= 0.3331	<i>m</i> = 0.5009	<i>m</i> = 0.669	93 m =	0.8360	<i>m</i> = 1.0040
0.00 ª	24 40	17 2	4 853	25 244	25 609	2	5 949	26,280
106.62	27.70	<i>n</i> 2	4.000 6.280	26.573	26.856	2	5.076	27.267
190.02	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	2	0.200 7.07E	20.0/0	20.000	21	7 971	21.201
396.29	27.32	20 2	1.215	27.538	27.806	2	1.0/1	20.123
595.97	27.60	25 2	8.129	28.369	28.601	20	5.051	28.873
795.65		2	8.857	29.086	29.309	2	9.331	29.536
895.49	29.38	30	_					-
995.33		2	9.498	29.716	29.897	2	9.930	<u> </u>
				$\phi_{V}(MgCl_{2})$				
P, bar	<i>m</i> = 0.00	m = 0.0	03505 n	n = 0.07877	<i>m</i> = 0.07937	m = 0.1395	<i>m</i> = 0.2184	<i>m</i> = 0.3150
0.00%				10.000	10.040	10.040	14.041	14 706
0.00*	11.1/	4 11.9	14	12.638	12.646	13.343	14.041	14.720
99.90	12.56	8 13.3	05	13.937	14.010	15.786	15.326	16.024
199.80	12.56	8 14.5	98	15.059		16.890	16.425	17.132
300.20	15.70	4 15.9	80		16.776	17.890		18.208
401.00	15.39	2 16.9	80	17.545	17.905	17.983	18.520	19.192
501 10	15.80	0 17.4	33	18 349	18 162	18.875	19.274	20.059
601.00	19.00	A 19.9	22	10.206	19.649		20.215	20.969
701.00	10.42	4 10.0	22	19.290	13.043	20.780	20.210	20.000
701.60		19.9	99	20.169	20.058	20.780	21.114	21.004
802.00	20.56	n —	-	21.332	21.6/7	21.730	21.799	
901.70			-	22.336	22.580	22.580	22.652	23.322
1001.20			-	22.955	22.973	23.446	23.336	
0 6			-	$\phi_{\vee}(Na_2SO_4)$	m = 0.1490	m = 0	0210	m = 0.3335
P, bar		m = 0.00899		- 0.0832	11 - 0.1480		2312	
0.00	) a	3.227		5.809	7.467	9.3	71	11.536
00.00	)	5 110		8.214	9.898	116	99	13.440
400.00		0.110		0 692	11 740	12 /	39	15 083
199.60				11 641	11.740	45 4	00	16 609
300,20		—		11.041		10.1	00 96	10.030
401.00	)			13.022	15.254	16./	00	10.1/0
501.10	)	11.805		14.365	16.626	18.1	/5	19.576
601.00	)	13.933		15.781	18.103	19.4	75	20.960
701.60	)	14.391		17.068	19.474	20.9	54	22.219
802.00	)	16.562		18.291	20.853	22.1	28	23.471
901 70	)	18,219		19.517	22,177	23.2	18	24.652
1001.00		.U.L 10			23.255	24.2	19	25.676
1001.20	<b>,</b> ,,,,,,,							
P har	m	≈ 0.01985	<i>m</i> = 0	φ <sub>∨</sub> (MgSO₄) .05328	m = 0.1029	<i>m</i> = 0 1	693	<i>m</i> = 0.2503
, odi			0					
0.00ª		9.081	<del>-</del> 7,	159	-5.568	-4.17	2	-2.881
196.62		-2.095	-	_	_			
296.95		_	-	_				—
396.29		1.140	2.	000	2.686	3.43	2	3.447
496 13		_		-	_			_
505.07		3 599	7	755	5 501	6.08	2	6.054
000.07 205.07		0.000	7.	,	0.001	0.00	-	
090.01			-	755	8 209	0 50	17	8 444
/ 95.05		0.400	7.	100	0.200	0.50		-
895.49				-	10.406		0	—
995.33		9.004	10.	191	10.490	10.76	2	

9.604 995.33 <sup>a</sup> The values of  $\phi_V$  have been normalized to the best available literature values calculated from eq 3.

Table II	The	Annovent Melal	Volumes of		Call Colutions of	Eurotion of	Concentration and	Brossure at 25 °	<b>^</b>
ladie II.	ine	Apparent Molal	volumes of	Aqueous	Salt Solutions as a	a Function of	concentration and	a Pressure at 25 v	-

			$\phi_{V}(NaC)$	21)			
P, bar	m = 0.1299	m = 0.2507	m = 0.3852	<i>m</i> = 0.7766	m = 0.9630	<i>m</i> = 1.3070	<i>m</i> = 2.008
0.00 <i>ª</i>	17.289	17.547	17.765	18.237	18.416	18.705	19,189
99.90	18.493	18.536	18.446	18.583	18.738	19.044	19.536
199.80	18.764	18.898	18.820	_	19.104	19.374	19.853
300.20	19.294	19.332	19.171		19.451	19.700	20.145
401.00	19.517	19.681	19.478	19.565	19.799	20.009	20.439
501.10	19.757	19.988	19.785	19.844	_	20.284	20.704
601.00	20.157	20.294	20.083	20.135	20.417	20.566	20.956
701.60	-	20,625	20.373	20.434	20.695	20.827	21.195
802.00	20.693	20.847	20.641	20.714	20.972	21.066	21.428
901.70	20.938		20.877	20.953	21.233	21.304	21.645
1001.20	31.133		21.131	—	21.462	21.524	

		$\phi_{\vee}($	<ci)< th=""><th></th><th></th></ci)<>		
P, bar	<i>m</i> = 0.3331	<i>m</i> = 0.5009	<i>m</i> = 0.6693	<i>m</i> = 0.8360	<i>m</i> = 1.0040
0.00 <i>ª</i>	27.935	28.193	28.415	28.610	28.791
196.62	28.873	29.104	29.258	29.249	29.467
396.29	29.470	29.670	29.867	29.804	30.000
595.97	29.985	30.189	30.319	30.287	30.465
795.65	30.434	30.628	30.752	30.712	30.896
995.33	30.789	31.015	31.137	31.080	31.257

		$\phi_{V}(MgCl_{2})$			
P, bar	m = 0.00876	m = 0.03505	<i>m</i> = 0.2184	m = 0.3150	
0.00 <i>ª</i>	15.172	15.781	17.162	17.477	
99.90	15.970	16.596	18.058	18.476	
199.80	_	17.140	18.825	19.250	
300.20	16.460	18.454	19.587	19.967	
401.00	16.664	18.812	21.199	20.692	
501.10		19.484	20.839	21.324	
601.00		19.806	21.537	21.977	
701.60	19.437	20.239	22.111	22.587	
802.00	21.241	21.693	22.640	23.129	
901.70	_	22.446	23.241	_	
1001.20		22.385	23.704	24.157	

		$\phi_{V}(Na_{2}SO_{4})$		
<i>P</i> , bar	<i>m</i> = 0.0832	<i>m</i> = 0.1480	<i>m</i> = 0.2312	<i>m</i> = 0.3335
0.00 <i>ª</i>	14.963	16.095	17.234	18.388
99.90	16.508	17.711	19.130	20.352
199.80	17.767	18.902	20.311	21.454
300.20	18.994	_	21.481	22.564
401.00	20.150	21.232	22.544	23.569
501.10	21.328	22.218	23.558	24.553
601.00	22.412	23.311	24.568	25.548
701.60	23.435	24.299	25.560	
802.00	24.569	25.332	26.494	27.394
901.70		26.255	27.415	_
1001.20		27.268	28.318	29.121

		$\phi_{ m V}({\sf Mg})$	SO4)			
P, bar	<i>m</i> = 0.01985	<i>m</i> = 0.05328	<i>m</i> = 0.1029	<i>m</i> = 0.1693	<i>m</i> = 0.2503	
0.00 <i>ª</i>	-3.402	-1.833	-0.660	0.346	1.375	
96.79			_	_		
196.62	1.861	3.089	3.653	4.598	4.351	
296.45						
396.29	4.569	5.626	_	6.774	6.443	
496.13					_	
595.97	6.614	7.840	8.008	8.777	8.395	
695.81	_					
795.65	7.543	9.769	9.864	10.580	10,150	
895.49					_	
995.33	9.148	11.431	11.570	12,204	11.801	

 $^a$  The values of  $\phi_{\rm V}$  have been normalized to the best available literature value calculated from eq 3.

Table III.	The Apparent N	folal Volumes	of Aqueous Salt	Solutions as a Fur	nction of Concentration	on and Pressure at 50	°C
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			¢√(NaCl)				
P, bar	<i>m</i> = 0.1299	<i>m</i> = 0.2507	m = 0.38	52	<i>m</i> = 0.7766	<i>m</i> = 0.9630	<i>m</i> = 1.307
0.00.4	18 610	18 865	19.060		19 4 16	19 527	19 677
99.90	19.718	19 545	19 648		19.917	19.838	19.954
199.80	20,090	10.040	10.040		20.203	20 127	20.222
300.30	20.090		19.942		20.203	20.137	20.232
401.00	20.430	20.125	20.242			20.422	20.492
401.00	20.698	20.393	20.533		20.731	20.705	20.950
501.10	20.858	20.686	20.793		20.987	20.971	_
601.00	21.154	21.029	21.048		21.205	21.224	21.223
701.60	21.339	21.348	21.306		21.448	21.470	21.442
802.00	21.607	21.601	21.612		21.699		21.666
901.70	21.742	21.964	21.881		21.893	—	21.868
1001.20	21.938	22.253	22.114		22.126		
			$\phi_{V}(KCI)$				
P, bar	<i>m</i> = 0.3331	<i>m</i> = 0.5009		m = 0.6693	3	<i>m</i> = 0.8360	<i>m</i> = 1.0040
0.00 <i>ª</i>	28.869	29.134		29.350		29.533	29.694
196.62	29.757	29.968		30.125		30.110	30.303
396.29	30.235	30,432		30.585		30.547	30.735
595.97		30.849		30,988		30.939	31 123
795.65	31.046			31 350		31 281	31.464
005 33	31 350	31 590		31 66 1		31 505	31 770
				31.001			
			$\phi_V(MgCl_2)$				
P, bar	<i>m</i> = 0.0	07937	m = 0.1395	5 	<i>m</i> = 0	.2184	<i>m</i> = 0.3150
0.00 <sup>a</sup>	15.6	21	16.229		16.7	'92	17.295
99.90	16.6	34	17.619		18.0	)23	18.317
199.80	17.2	38	18.261		18.7	/17	19.028
300.20	18.1	05	18.974		19.4	54	19.747
401.00	18.5	12	19.546		20.1	18	20.353
501 10	19 1	85	20 206		20.7	709	21.010
601.00	19.9	16	20.645		21.3	356	21.602
701.60	20.5	44	21 246		21 9	17	
802.00	20.8	44	21.755		22.5	531	22.705
<u></u>							
P. bar	m = 0.00899	<i>m</i> = 0.0367	$\phi_V(Na_2SO_4)$ m = 0.0832	? n	n = 0.1480	m = 0.2312	<i>m</i> = 0.3335
· · · · · · · · · · · · · · · · · · ·							
0.00 <i>ª</i>	15.256	16.428	17.584		18.714	19.826	20.925
99.90		16.478	18.726		19.787	20.905	21.982
199.80	16.371	17.563	19,717		20.849	21.904	22.975
300.20	18.017	—	20.918		21.810	22.910	23.912
401.00	19.114	19.650			22.679	23.847	24.779
501.10		20.563	22.703		23.630	24.705	25.624
601.00		21.341	23.567		24.487	25.516	26.440
701.60	22.358	22,503	24.323		25.329	26.365	27.230
802.00	22.799	22.997			26.129	27.075	28.008
			. (M-00 )				
P har	m = 0.01985	m = 0.0532	<i>ψ</i> γ(ivigο∪₄) 28	m = 0.10	29	<i>m</i> = 0,1693	m = 0.2503
0.00 <i>ª</i>	-2.861	-1.053		0.073		0.973	2.068
196.62	2.783	4.211		4.564		5.191	5.025
396.29	6.012	6.784		6.764		7.185	6.933
496.13							-
595.97	8 345	8 730		8.500		8.979	8.643
605 21	0.040	0.700					_
705 65	0 106	10 220		0 004		10 5 1 5	10.140
190.00	3,430	10.229		3.304			
070.49		_		11 400		11 777	11 535
995.33	9.979			11.420		11.777	11.000

 $^a$  The values of  $\phi_V$  have been normalized to the best available literature values calculated from eq 3.

### **Results and Discussion**

The densities of aqueous solutions of NaCl, KCl, MgCl<sub>2</sub>, Na<sub>2</sub>SO<sub>4</sub>, and MgSO<sub>4</sub> have been measured (*2*) from 0.01 to 1.0 ionic strength with a high pressure densimeter. The measurements were made from 0 to 1000 bars (in 100 bar increments)

and at 0, 25, and 50  $^{\circ}$ C. The apparent molal volumes have been determined from these densities (*d*) by using the equation

$$\phi_{\rm V} = \frac{1000(d^0 - d)}{dd^0 m} + \frac{M}{d} \tag{1}$$



Figure 1. Apparent molal volumes of NaCl as functions of pressure at various concentrations and 0  $^{\circ}{\rm C}.$ 



**Figure 2.** Apparent molal volumes of NaCl, KCl, MgCl<sub>2</sub>, Na<sub>2</sub>SO<sub>4</sub>, and MgSO<sub>4</sub> as functions of pressure at  $l_m \approx 1$  and 0 °C.

where  $d^0$  is the density of water (4), *m* is the molality of the solution, and *M* is the molecular weight of the salt. The values of  $\phi_V$  determined from eq 1 are given in Tables I, II, and III for various solutions. Since the  $\phi_V$ 's for NaCl solutions have been obtained over the largest concentration range (0.03 to 2 *m*), we have examined the pressure and concentration dependence in Figure 1. The values of  $\phi_V$  for NaCl at various molal ionic strengths,  $I_m$ , are plotted vs. pressure. The  $\phi_V$ 's increase with increasing pressure over the entire concentration range studied. At low molalities the  $\phi_V$ 's show a nonlinear pressure dependence. This behavior is similar at each temperature for all of the electrolytes studied (see Figure 2).

Although the concentration dependences for some of the electrolytes studied are not linear functions of  $m^{1/2}$  at a given pressure (Figure 3), the relative apparent molal volumes,  $\phi_V(P) - \phi_V(0)$ , are linear functions of  $m^{1/2}$  (see Figure 4). Since the high pressure magnetic float system was designed to study the pressure effect on the densities or apparent molal volumes, we examined the relative apparent molal volumes as a function of applied pressure P (at P = 0, the absolute pressure is 1 atm), temperature (°C), and concentration (m, mol/kg of H<sub>2</sub>O) by using the linear equation





**Figure 3.** Apparent molal volumes of NaCl, KCl, MgCl<sub>2</sub>, Na<sub>2</sub>SO<sub>4</sub>, and MgSO<sub>4</sub> as functions of  $m^{1/2}$  at 0 °C and 1000 bars.



**Figure 4.** Relative apparent molal volumes,  $\phi_V(P) - \phi_V(0)$ , for NaCl, KCl, MgCl<sub>2</sub>, Na<sub>2</sub>SO<sub>4</sub>, and MgSO<sub>4</sub> as functions of  $m^{1/2}$  at 0 °C and 1000 bars.

where  $\phi_V(P)$  and  $\phi_V(0)$  are the apparent molal volumes at applied pressure, *P* and 0; the superscript zero is used to denote infinite dilution; and *S* is an empirical parameter that varies with pressure and temperature. The relative infinite dilution apparent molal volumes and the parameter *S* were fitted by using a least-squares method to equations of the form

$$\phi_{\rm V}{}^{\rm 0}(P) - \phi_{\rm V}{}^{\rm 0}(0) = \sum_{i,j}^n a_{i,j} P^i t^j$$
 (2a)

$$S = \sum_{i,j}^{n} b_{i,j} P^{i} t^{j}$$
(2b)

The coefficients needed for eq 2a and 2b were arrived at by fitting the data on an UNIVAC 1106 computer. These coefficients are given in Table IV along with the standard deviations.

In order to calculate the  $\phi_V$  at a given *P*, *t*, and *m* from these equations, it is necessary to have reliable  $\phi_V$  data at 1 atm or P = 0. The "best" available literature values for the 1 atm apparent molal volumes have been selected (1, 5–7, 10, 14, 17) and were fitted to the equation

$$\phi_{\rm V}(0) = \phi_{\rm V}^{0}(0) + Am^{1/2} + Bm + Cm^{3/2} \tag{3}$$

where  $\phi_{\vee}^{0}(0)$ , *A*, *B*, and *C* are all temperature dependent parameters

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Variables	NaCl	KCI	MgCl <sub>2</sub>	Na <sub>2</sub> SO <sub>4</sub>	MgSO₄
P	1.542 (E — 2)	1.228 (E — 2)	1.566 (E — 2)	2.285 (E — 2)	4.076 (E -2)
Pt	-1.099 (E - 4)	-1.589 (E-4)	-3.150 (E - 4)	-3.141 (E - 4)	-2.901 (E - 4)
Pt <sup>2</sup>	9.68 (E - 7)	1.797 (E - 6)	3.911 (E - 6)	2.125 (E - 6)	5.888 (E - 6)
Pm <sup>1/2</sup>	-7.62(E-3)	-6.964 (E - 3)	-2.269 (E - 3)	-1.576 (E - 3)	-3.887 (E - 2)
Ptm <sup>1/2</sup>	3.05 (E - 6)	7.060 (E - 5)	2.611 (E - 4)	1.257 (E - 4)	3.066 (E - 4)
$Pt^2m^{1/2}$	0	-9.849 (E - 7)	-3,115 (E - 6)	-1.597 (E - 6)	-9.099 (E - 6)
p <sup>2</sup>	-2.439 (E - 5)	-1.261(E - 5)	-1.202 (E - 5)	-1.250 (E - 5)	-3.593 (E - 5)
$P^2t$	1.81 (E - 8)	1.19 (E - 8)	1.19 (E - 8)	6.92 (E - 8)	-1.273 (E - 7)
$P^2 m^{1/2}$	1.415 (E - 5)	1.089 (E - 5)	-3.14 (E - 6)	-3.11(E - 6)	4.239 (E - 5)
P <sup>2</sup> tm <sup>1/2</sup>	0	0	0	0	2.261 (E - 7)
<b>p</b> <sup>3</sup>	2.158 (F - 8)	6.50 (E - 9)	1.496 (E - 8)	9.82 (F - 9)	1.567 (E - 8)
$P^3m^{1/2}$	-8.11 (E - 9)	-6.26 (E - 9)	-5.3 (E - 11)	0	-1.662 (E - 8)
P <sup>4</sup>	-6.48 (E - 12)	0	-6.54 (F $- 12$ )	-3.08 (F - 12)	0
Std dev	0.23	0.08	0.18	0.24	0.28

<sup>a</sup> The terms (E – a), given for each variable, mean the coefficient is times  $10^{-a}$ .

Table V. Coefficients for Equation 3<sup>a</sup>

Variables	NaCl	KCI	MgCl <sub>2</sub>	Na₂SO₄	MgSO <sub>4</sub>
φγ <sup>0</sup> , <sub>1 atm</sub> 0 °C	12.90	23.63	10.42	2.33	- 13.06
t	0.1990	0.1788	0.2660	0.508	0.3720
t <sup>2</sup>	-2.008 (E - 3)	-2.000 (E - 3)	-4.128 (E - 3)	-5.456 (E - 3)	-5.472 (E - 3)
m <sup>1/2</sup>	1.5992	1.407	8.132	8.188	33.3710
tm <sup>1/2</sup>	5.388 (E - 3)	1.118 (E — 2)	-0.0498	0.1777	-0.2963
$t^2 m^{1/2}$	2.194 (E - 4)	1.848 (E - 4)	1.277 (E - 3)	-1.8704 (E - 3)	1.314 (E - 2)
m	1.004	1.235	-0.820	13.427	-40.4948
tm	-4.951 (E - 2)	-5.714 (E - 2)	-0.2202	-0.7505	-4.843 (E - 2)
t²m	3.082 (E - 4)	5.256 (E - 4)	3.382 (E - 3)	9,2568 (E - 3)	-2.821 (E - 2)
$m^{3/2}$	0	0 ` ′	0	0	28.8998
tm <sup>3/2</sup>	0	0	0	0	0.2388
$t^2 m^{3/2}$	0	0	0	0	2.482 (E - 2)
Av dev	0.051	0.01 <sub>0</sub>	0.03 <sub>3</sub>	<b>0.04</b> <sub>1</sub>	0.028

<sup>a</sup> The terms (E – a), given for each variable, mean the coefficient is times  $10^{-a}$ .

$$\phi_{\vee}^{0}(0) = \sum_{i}^{n} \phi_{i} t^{i}$$
(3a)

$$A = \sum_{i}^{n} A_{i} t^{i}$$
(3b)

$$B = \sum_{i}^{n} B_{i} t^{i}$$
 (3c)

$$C = \sum_{i}^{n} C_{i} t^{i}$$
(3d)

The coefficients for eq 3 are given in Table V along with the standard deviations.

The temperature effect on the apparent molal volumes at 1000 bars and  $l_{\rm m} = 1$  is shown in Figure 5. The values of  $\phi_{\rm V}$  for NaCl and KCl increase with temperature, the values of  $\phi_{\rm V}$  for MgCl<sub>2</sub> have small temperature effects, while  $\phi_{\rm V}$ 's for Na<sub>2</sub>SO<sub>4</sub> increase rapidly at temperatures between 0 and 30 °C, then start to level off and have a tendency to decrease at temperatures above 40 °C. The values of  $\phi_{\rm V}$  for MgSO<sub>4</sub> actually show a maximum at 30 °C.

The smoothed apparent molal volumes of these electrolytes calculated from eq 2 and 3 can be used to calculate the densities by using the equation

$$d = d^{0}(1000 + mM)/(d^{0}m\phi_{V} + 1000)$$
(4)

The average errors in  $\phi_{\rm V}$  for NaCl at 1000 bars are approximately  $\pm 0.1$  (at  $l_{\rm m} = 1.0$ ) and  $\pm 0.2$  (at  $l_{\rm m} = 0.1$ ) cm<sup>3</sup> mol<sup>-1</sup>, which correspond to density errors of  $\pm 100$  and  $\pm 20$  g cm<sup>-3</sup>, respectively. The density errors for other salts are smaller.



**Figure 5.** Apparent molal volumes of NaCl, KCl, MgCl<sub>2</sub>, Na<sub>2</sub>SO<sub>4</sub>, and MgSO<sub>4</sub> as functions of temperature at  $I_m = 1$  and 1000 bars.

The apparent molal compressibilities can be calculated by differentiating eq 1 with respect to pressure

$$\phi_{\rm K} = -\partial \phi_{\rm V} / \partial P \tag{5}$$

The values of  $\phi_{\rm K}$  for NaCl, MgCl<sub>2</sub>, and Na<sub>2</sub>SO<sub>4</sub> calculated at  $l_{\rm m}$  = 1.0, 0 °C, and 1 atm agree reasonably with the data of Millero

Table VI. Comparisons of  $\phi_{\mathbf{K}}$  Obtained in this Study and the Data of Millero et al. at  $I_m = 1.0, 0$  °C, and 1 Atm

Salt	$-10^4\phi_{K}$ (ours)	−10 <sup>4</sup> φ <sub>K</sub> <sup>a</sup> (Millero et al.)
NaCl	78 ± 28	60.4
MgCl <sub>2</sub>	143 ± 22	121.2
Na <sub>2</sub> SO <sub>4</sub>	219 ± 29	171.4
MgSO₄	213 ± 24	156.4
Millero et al. (16)	, eq. 10.	

et al. (16) (Table VI). The result of MgSO<sub>4</sub> is higher than the data of Millero et al.

Currently, the atmospherical densities and heat capacities of the major sea salts are being measured over a wide temperature range in our laboratory. Also the high pressure sound speed in the aqueous solutions of the major sea salts is being measured; these new results will be combined with the atmospherical densities and heat capacities to give precise equations of state for the major sea salts. The apparent molal volumes and compressibilities calculated from the sound-derived equations of state will be compared with the results of this study.

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## Preliminary Data on the Pressure Effect on the Viscosity of Sodium Chloride–Water Solutions in the Range 10–40 °C

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The paper describes new, and preliminary, measurements of the viscosity of NaCl solutions in H<sub>2</sub>O over a range of temperatures 10–40  $^\circ\text{C},$  a range of pressures 0–30.0 MPa, and at three concentrations, together with check measurements on pure water. The precision is 0.2% and the accuracy is 0.3%. The measurements are represented by a purely empirical, analytic correlation which reproduces the ensemble of data with a standard deviation of 0.2%.

In conjunction with the expanding national program of research and development in geothermal energy, White and Williams (27), ERDA (2), it becomes increasingly more important to have access to a variety of thermophysical data concerning brines. In this connection the viscosity plays an important role, because it is needed to calculate pressure losses in wells, ducts, and channels, and, even more importantly, it is essential for the determination of porosities of rocks. Finally, the possibility that Walden's rule, Erdey-Grúz (3), may be applicable, opens the prospect of replacing the measurement of equivalent electric conductance by the, usually simpler, measurement of viscosity

In order to make a contribution to the solution of this problem, we have organized a program of measurement of the viscosity of a number of brines as a function of pressure, temperature, and composition. The measurements are performed in a slightly modified oscillating-disk viscometer, Kestin and Moszynski (13) and Kestin and Leidenfrost (10), which has been successfully

used in the past for the determination of the viscosity of compressed water, Moszynski (19), as well as superheated steam, Kestin and Wang (16) and Kestin and Richardson (14).

It is natural that a program of measurements on a variety of ionic solutions should start with solutions of sodium chloride. The present paper contains a very preliminary account of our results in the range of temperatures 10-40 °C, in the pressure range 0-30.0 MPa (MPa =  $10^6$ N/m<sup>2</sup> = 10 bar = 145.04 psi), and over a range of compositions up to about 90% of saturation.

The viscosity of sodium chloride solutions has been measured by a number of investigators, notably by Kaminsky (5). Survanarayana and Venkatesan (24), Korosi and Fabuss (17), Lengyel (18), Ostroff, Snowden, and Woessner (20), and Werblan, Rotowska, and Minc (26). Data are also listed in the book by Stokes and Mills (23). The measurements available in the literature cover the full range of compositions and a range of temperatures up to 150 °C; they all seem to have been performed by the capillary-flow method, and almost exclusively with the aid of an Ubbelohde-Rankine type of viscometer. However, as far as pressures are concerned, we were unable to locate any measurements at pressures higher than about 1.4 MPa, Potter, Shaw, and Haas (21). The fact that ours seem to be the first measurements which throw light on the effect of pressure on the viscosity of concentrated ionic solutions has provided the motivation for the preparation of this preliminary account. A more detailed report is reserved for a future date.

### 2. The Method

The data on the viscosity of NaCI-H<sub>2</sub>O solutions described in this paper have been obtained in an oscillating-disk instrument.